

## Effect of Magnesium Fluoride in Chromium–Magnesium Catalysts on the Fluorination Reaction of 1,1,1-Trifluoro-2-chloroethane

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Magnesium fluoride, mixed with chromium fluoride, enhances the activity, selectivity and lifetime of the chromium catalyst for the vapour-phase fluorination of CF<sub>3</sub>CH<sub>2</sub>Cl with anhydrous HF to give CF<sub>3</sub>CH<sub>2</sub>F.

CF<sub>3</sub>CH<sub>2</sub>F (HFC-134a) is considered as one of the most promising candidates for the substitution of CFC-12 (CF<sub>2</sub>Cl<sub>2</sub>).<sup>1,2</sup> One of the synthetic routes to HFC-134a is the vapour-phase fluorination of CF<sub>3</sub>CH<sub>2</sub>Cl (HCFC-133a) with HF over Cr- or Al-based catalysts. Among various fluorination catalysts, the characteristics of Cr<sub>2</sub>O<sub>3</sub> have been extensively examined.<sup>3–6</sup> However, Cr<sub>2</sub>O<sub>3</sub> has been found rapidly deactivated during the fluorination of HCFC-133a, which is a major drawback in its industrial application.

We initially assumed that only a small portion of the surface chromia was fluorinated, which could be the reason for the fast deactivation of Cr<sub>2</sub>O<sub>3</sub>. CrF<sub>3</sub>·4H<sub>2</sub>O was chosen as the catalyst precursor on the assumption that high fluorine-containing catalysts might have better catalytic activity and a longer lifetime. Cylindrical extrudates of CrF<sub>3</sub>·4H<sub>2</sub>O (30 g) were loaded in an Inconel 600 reactor, dried *in situ* at 400 °C for 1 h under He, then activated with HF at 200 °C for 2 h, and at 400 °C for 1 h. The fluorination reaction was conducted at 360 °C at atmospheric pressure. Contrary to our expectation, the fluorination of HCFC-133a with HF over CrF<sub>3</sub>·4H<sub>2</sub>O gave only a small amount of the desired product, HFC-134a, in 1.5% yield and an appreciable amount of an unwanted product, CF<sub>2</sub>=CHCl, (HCFC-1122) in 1.1% yield.

Since CrF<sub>3</sub>·4H<sub>2</sub>O had a small specific surface area (8 m<sup>2</sup> g<sup>-1</sup>), we mixed MgF<sub>2</sub>, which is inactive for the fluorination of HCFC-133a, with CrF<sub>3</sub>·4H<sub>2</sub>O to increase the surface area of the catalyst. Surprisingly, the catalytic activity increased significantly, by more than 11 times the amount when CrF<sub>3</sub>·4H<sub>2</sub>O was used alone, even though the surface area of the catalyst increased by only four times (Table 1). Furthermore, the formation of HCFC-1122, which is known to be responsible for the deactivation of Cr catalysts, was significantly reduced, to less than 0.05%. Variation in molar composition of the mixed catalyst, ranging from CrF<sub>3</sub>·4H<sub>2</sub>O:MgF<sub>2</sub> = 0.1 to 10, showed only a slight difference in the fluorination activities. In addition, unlike Cr<sub>2</sub>O<sub>3</sub>, the catalytic activities of the mixtures remained almost unchanged with the reaction time up to 200 h at 360 °C.

As shown in Fig. 1, the XRD pattern of the mixture of CrF<sub>3</sub>·4H<sub>2</sub>O and MgF<sub>2</sub> is different from that of CrF<sub>3</sub>·4H<sub>2</sub>O, indicating the formation of new chromium species. In addition,

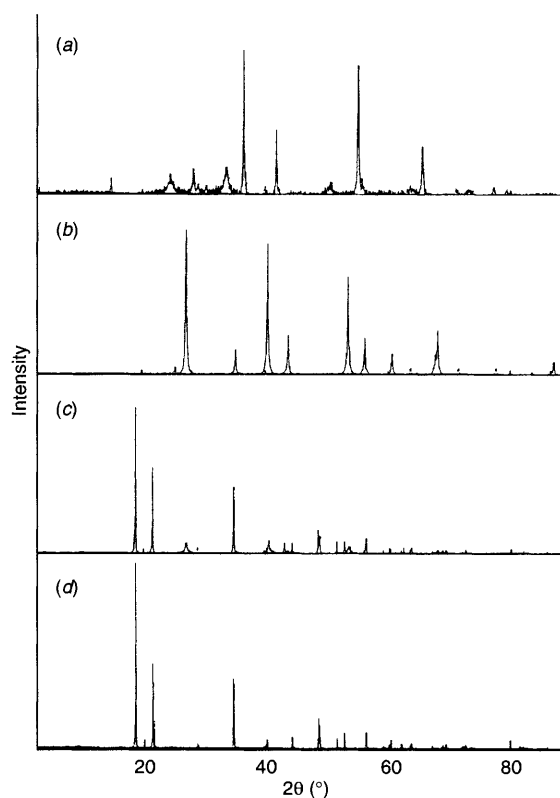
the crystallinity of MgF<sub>2</sub> is markedly reduced when mixed with CrF<sub>3</sub>·4H<sub>2</sub>O. This suggests that a large portion of MgF<sub>2</sub> exists in an amorphous state when in the mixture. The newly formed chromium species is presumed to be CrF<sub>3</sub>·3H<sub>2</sub>O by comparing its XRD pattern with the XRD pattern of authentic CrF<sub>3</sub>·3H<sub>2</sub>O as well as with the standard XRD pattern in the library. Without the addition of MgF<sub>2</sub>, the new chromium species was not obtained by the thermal treatment of CrF<sub>3</sub>·4H<sub>2</sub>O in N<sub>2</sub> or in air up to 360 °C. Another new possible species proposed is a Mg–Cr salt such as MgCrO<sub>x</sub>F<sub>y</sub>,<sup>7</sup> which potentially forms in the mixture of CrF<sub>3</sub>·4H<sub>2</sub>O and MgF<sub>2</sub>. These new Cr-containing species could be the active centre for the fluorination reaction.

Solid-state <sup>19</sup>F NMR spectroscopy was applied to CrF<sub>3</sub>·4H<sub>2</sub>O, and to the mixture of CrF<sub>3</sub>·4H<sub>2</sub>O and MgF<sub>2</sub> to help identify the new chromium species in the mixture. However, the spectra of the solids did not show any difference in the samples, due to the very poor spectral resolution. As both CrF<sub>3</sub>·4H<sub>2</sub>O and the mixture of CrF<sub>3</sub>·4H<sub>2</sub>O and MgF<sub>2</sub> were slightly soluble in water, <sup>19</sup>F NMR spectra were taken in D<sub>2</sub>O with CF<sub>3</sub>CO<sub>2</sub>D as an internal standard. The spectrum of CrF<sub>3</sub>·4H<sub>2</sub>O shows four peaks at δ -51.761, -67.458, -73.040 and -88.278, while the mixture gives only three peaks at δ -50.625, -65.539 and

**Table 1** Product distribution of HCFC-133a fluorination

Molar ratio of CrF <sub>3</sub> :MgF <sub>2</sub>	Surface area of catalyst/m <sup>2</sup> g <sup>-1</sup> <sup>a</sup>	Product distribution (mol%)	
		HFC-134a	HCFC-1122
CrF <sub>3</sub> alone	8	1.5	1.1
10:1	31	16.9	0.6
5:1	47	17.8	0.3
1:1	79	20.7	0.0
0.5:1	84	21.1	0.0
0.25:1	93	20.7	0.0
0.1:1	94	19.4	0.0
MgF <sub>2</sub> alone	102	0.7	0.2

<sup>a</sup> Specific surface area of the catalysts measured before the fluorination reaction



**Fig. 1** XRD Powder patterns of (a) CrF<sub>3</sub>·4H<sub>2</sub>O (×5), (b) MgF<sub>2</sub> (×1), (c) the mixture of CrF<sub>3</sub>·4H<sub>2</sub>O and MgF<sub>2</sub> (molar ratio of Cr:Mg = 1:2, ×1), (d) CrF<sub>3</sub>·3H<sub>2</sub>O (×3)

–72.806. This result again indicates that the chromium species in the mixture is different from  $\text{CrF}_3 \cdot 4\text{H}_2\text{O}$ .

Brunet<sup>5</sup> and Coulson<sup>8</sup> reported that the catalytic activity of  $\text{Cr}_2\text{O}_3$  is proportional to the number of chromium atoms having an oxidation state higher than three. Measurement of the high-valent ( $> + 3$ ) chromium by titration technique showed that both  $\text{CrF}_3 \cdot 4\text{H}_2\text{O}$  and the mixture of  $\text{CrF}_3$ – $\text{MgF}_2$  have negligible oxidizing capacities, *ca.*  $5.5 \times 10^{-5} \text{ F g}^{-1}$  of catalyst. This result could indicate that the active sites of  $\text{CrF}_3$ – $\text{MgF}_2$  for fluorination are not closely related to the amount of the high-valent chromium species existing on the catalyst's surface.

From the above results it is deduced that besides increasing the catalyst's surface area,  $\text{MgF}_2$  plays an important role in lengthening the lifetime of the chromium catalyst by suppressing the formation of  $\text{CF}_2=\text{CHCl}$ . In addition,  $\text{MgF}_2$  enhances the fluorination activity, possibly through an electronic interaction with  $\text{CrF}_3$  or by forming a new metal salt such as  $\text{MgCrO}_x\text{F}_y$ .

Electronic spectroscopy in chemical analyses studies are under way to elucidate the role of  $\text{MgF}_2$  and to characterize the active chromium species. Fluorination activities are also under

examination with various forms of  $\text{MgCrO}_x\text{F}_y$ , which might be prepared from various  $\text{CrO}_x\text{F}_y$  and  $\text{MgF}_2$ .

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